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# Research and Development of Biomass Conversion Technologies in Shanghai JiaoTong University, China

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1. Introduction to Shanghai JiaoTong University(SJTU)
  2. Biomass characteristics
  3. Biomass fast pyrolysis for bio-oil production
  4. Biochar Application for Soil Amendment
  5. Gasification
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  7. Biogas technology
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-



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Shanghai Jiao Tong University

# 1.Shanghai JiaoTong University(SJTU)

- ◆ Established in 1896
- ◆ There are 20 schools, including school of Agriculture and Biology, School of Mechanical and Power Engineering, School of Environment Engineering, etc.
- ◆ Students:44020; Teachers:2851
- ◆ Area of campus: about 333 ha.





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## School of Agriculture and Biology (SJTU)

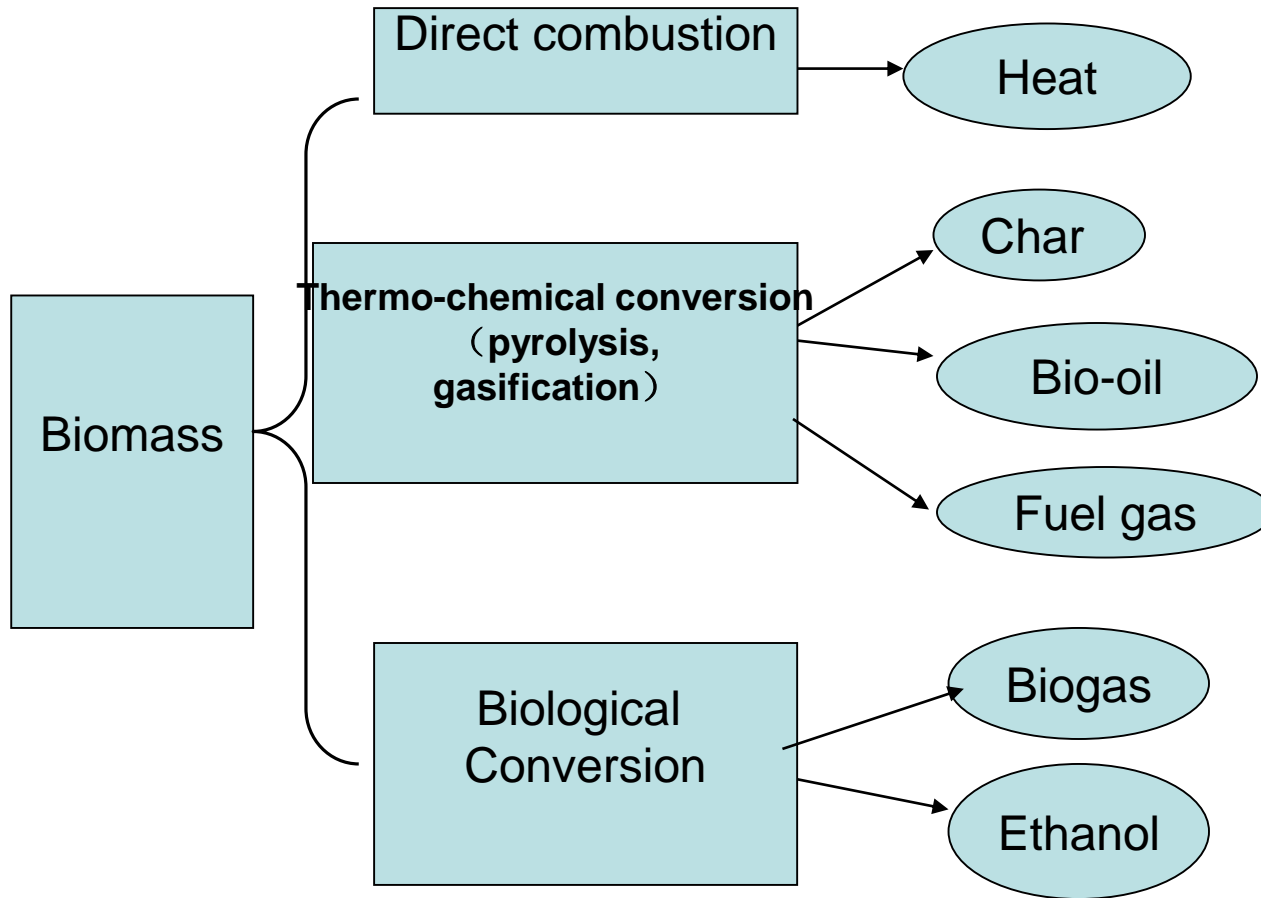
Biomass Energy Engineering Research Centre,

School of Agriculture and Biology , Shanghai JiaoTong University has a lot of experiences in the field of biomass energy and environment.

Including characterization of biomass, biomass pyrolysis, biochar, gasification, bioethanol, biogas, etc.









## 2. Research on biomass characteristics

**Objective:** To establish database of biomass characteristics and provide a theoretical basis for utilization of biomass.

**Sample source:**

- 1) Various areas: Shanghai, Anhui and Jiangxi;
- 2) Various agricultural residue: Rice straw, wheat straw, corn stalk, rape straw and cotton stalk.

Samples: 275 samples;

- 3) Various manure: Pig, broiler, layer, dairy cow and beef.
- Samples: 275 samples.



# Characteristics of agricultural biomass: elemental analysis

## Elemental analysis of livestock and poultry manure/%

	Manure of layer	Manure of pig	Manure of dairy cow
C	$37.863 \pm 1.501$	$38.695 \pm 2.801$	$40.485 \pm 0.904$
H	$5.107 \pm 0.501$	$6.068 \pm 0.437$	$5.982 \pm 0.238$
N	$2.705 \pm 0.762$	$2.508 \pm 0.355$	$2.120 \pm 0.068$
S	$0.514 \pm 0.051$	$0.755 \pm 0.038$	$0.532 \pm 0.075$
O	$53.812 \pm 1.273$	$51.975 \pm 3.551$	$50.880 \pm 1.172$

## Elemental analysis of stalk and straw/%

	Rice straw	Corn stalk	Rape straw	Cotton stalk
C	$40.745 \pm 1.426$	$41.811 \pm 2.843$	$38.618 \pm 1.433$	$43.993 \pm 1.488$
H	$5.644 \pm 0.326$	$5.868 \pm 0.517$	$5.737 \pm 0.383$	$5.877 \pm 0.372$
N	$0.906 \pm 0.362$	$1.35 \pm 0.358$	$0.456 \pm 0.215$	$1.233 \pm 0.46$
S	$0.815 \pm 1.581$	$0.367 \pm 0.045$	$0.932 \pm 0.225$	$0.417 \pm 0.16$
O	$46.81 \pm 5.434$	$47.587 \pm 2.409$	$54.257 \pm 1.598$	$48.317 \pm 1.209$

# Basic properties of agricultural biomass: proximate analysis

## Proximate analysis of livestock and poultry manure /%

	Manure of layer	Manure of pig	Manure of dairy cow
Moisture	$60.83 \pm 2.58$	$74.11 \pm 3.71$	$81.31 \pm 1.88$
Crude ash	$21.35 \pm 3.34$	$21.07 \pm 5.13$	$13.40 \pm 2.09$
Volatile	$54.89 \pm 6.11$	$56.49 \pm 3.63$	$59.75 \pm 2.20$
Fixed carbon	$15.73 \pm 1.19$	$13.51 \pm 1.05$	$17.97 \pm 4.25$

## Proximate analysis of stalk and straw /%

	Rice straw	Corn stalk	Rape straw	Cotton stalk
Moisture	$4.21 \pm 0.67$	$5.46 \pm 3.30$	$4.23 \pm 1.52$	$3.13 \pm 1.44$
Crude ash	$14.00 \pm 1.23$	$5.84 \pm 1.75$	$7.66 \pm 0.83$	$6.63 \pm 0.15$
Volatile	$67.49 \pm 2.04$	$71.79 \pm 5.93$	$74.63 \pm 0.86$	$71.89 \pm 1.24$
Fixed carbon	$14.29 \pm 0.29$	$16.92 \pm 1.59$	$13.48 \pm 2.27$	$18.35 \pm 0.74$





### 3. Biomass fast pyrolysis for bio-oil production

#### Mechanism of biomass pyrolysis

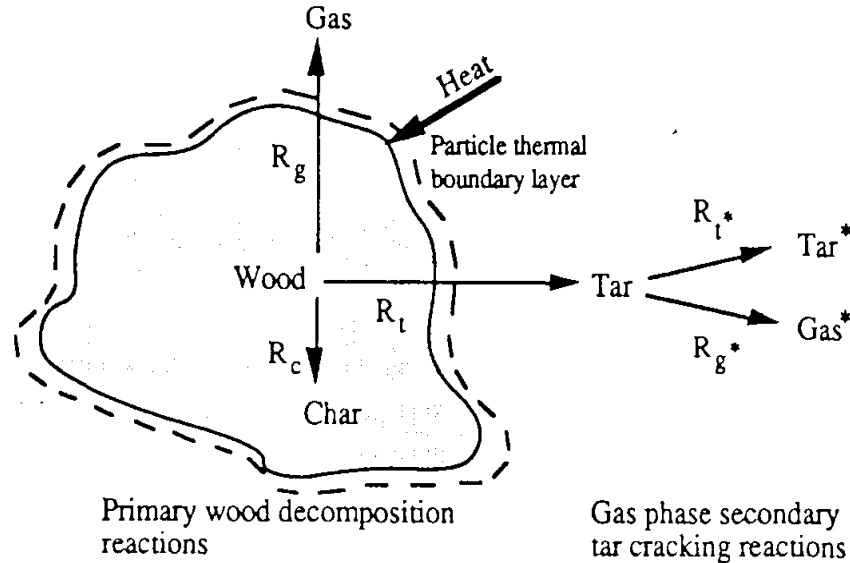


Fig.1 Sketch of a Decomposing Wood Particle  
Including the Reaction Paths Involved

**If the pyrolysis conditions are proper, 100kg biomass can produce 60 kg bio-oil.**



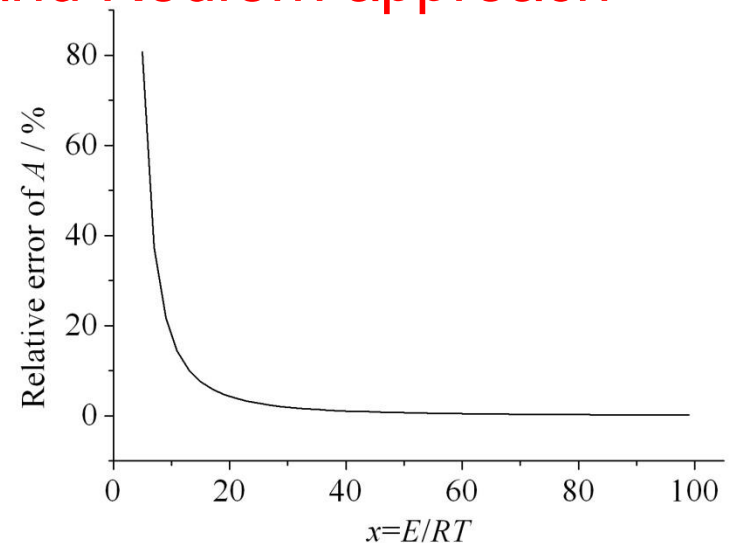
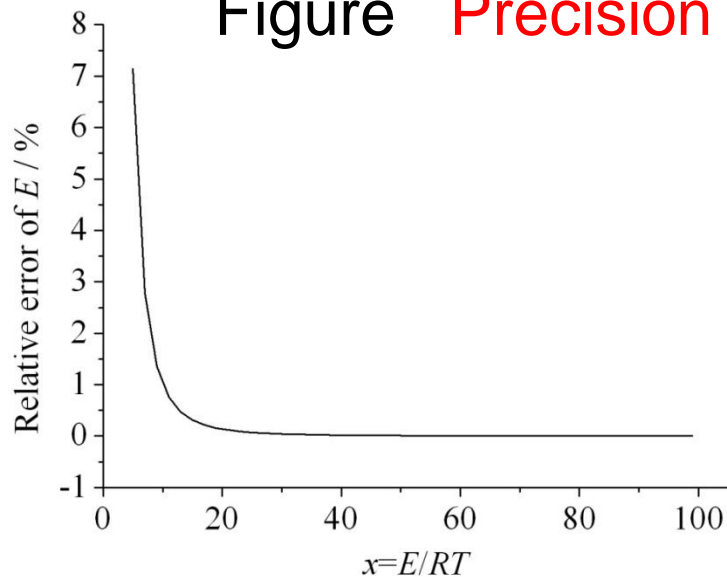
- Relative error of activation energy obtained by integral methods

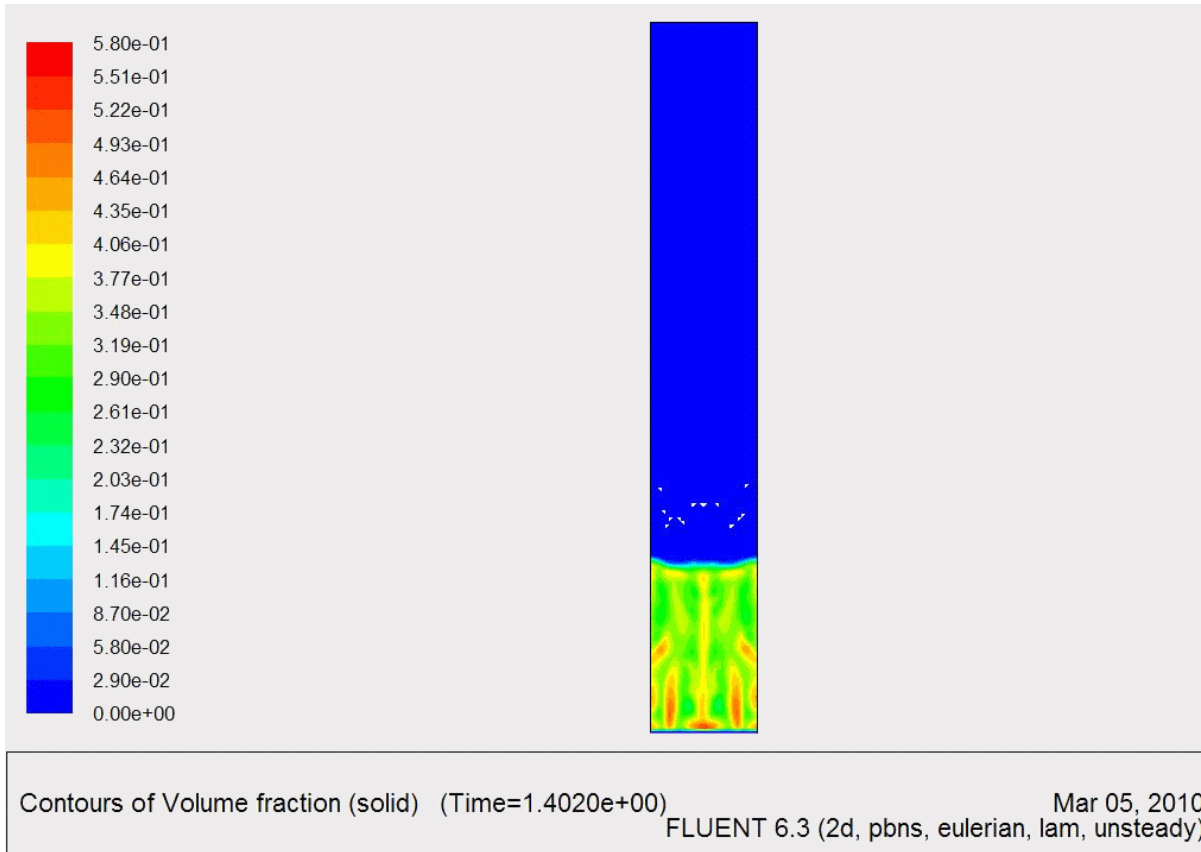
$$(\varepsilon_E + 1) \left( 1 - \frac{d \ln h_1 [(\varepsilon_E + 1)u]}{d [(\varepsilon_E + 1)u]} \right) = 1 - \frac{d \ln h(u)}{du}$$

- Relative error of frequency factor obtained by integral methods

$$\varepsilon_A = (\varepsilon_E + 1) e^{\varepsilon_E u} \frac{h(u)}{h_1 [(\varepsilon_E + 1)u]} - 1$$

Figure Precision of Coats and Redfern approach





Result: when time  
is 4 s, the  
fluidization of sand  
is best

Simulation of sand in fluidized bed reactor



# Fluidized bed reactor for biomass fast pyrolysis for bio-oil production developed by Shanghai JiaoTong University

Biomass  
throughput: 1-5  
kg/h;

Reactor  
Temperature: 400-  
600° C

Biomass particle  
size: 1-2mm





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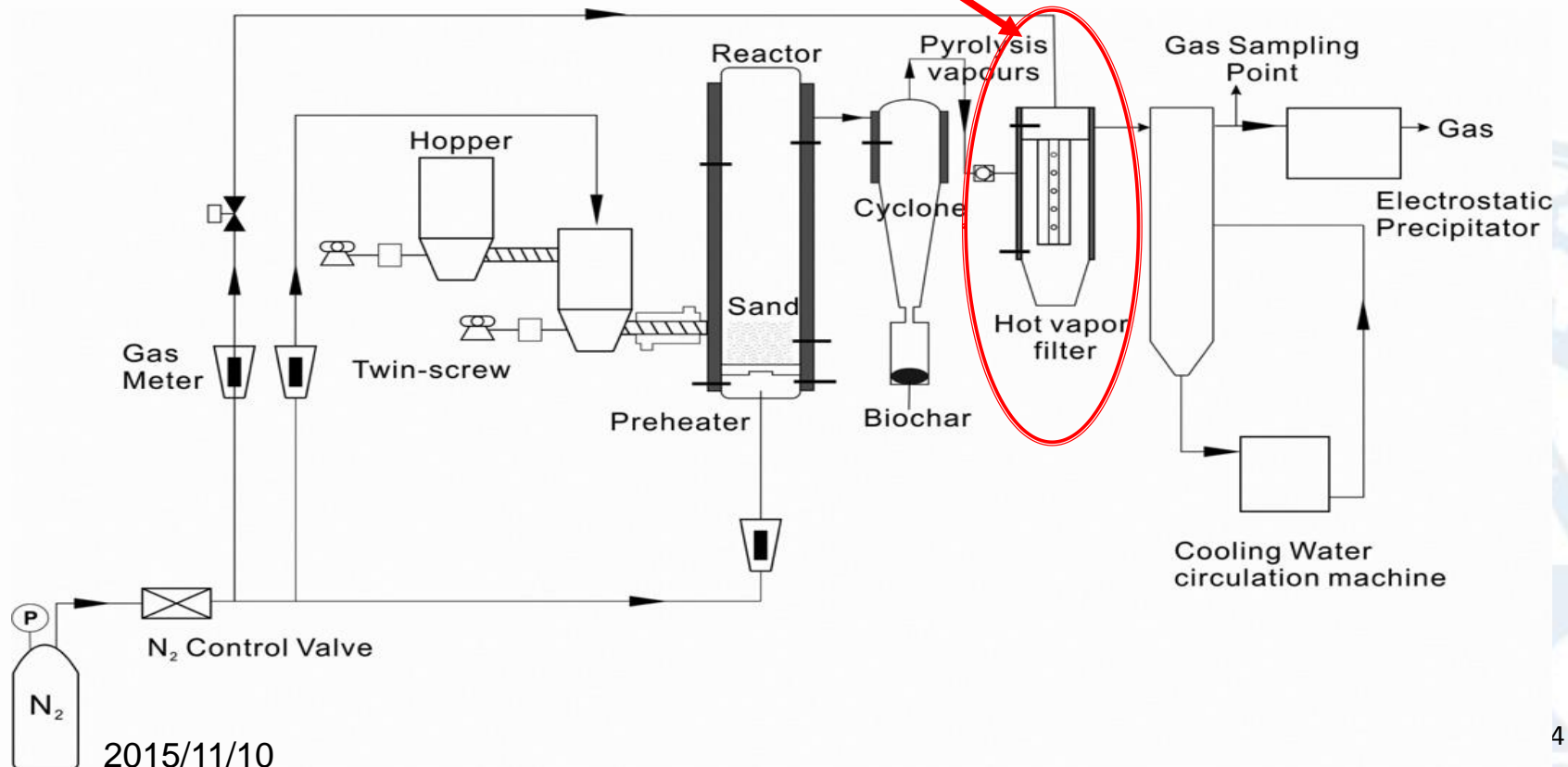
Bio-oil from stalk by fast pyrolysis (National Natural Science Foundation of China , Coordinated by Prof.Liu Ronghou, Biomass Energy Lab. SJTU)

# 秸秆 生物油





# \*Effect of hot vapor filtration on the characterization of bio-oil from rice husks with fast pyrolysis in a fluidized-bed reactor





# Yield and physicochemical properties of bio-oil at condenser

Yield and physicochemical properties of the bio-oil at the condenser and the EP.

	C <sub>1</sub> <sup>c</sup>	C <sub>2</sub> <sup>c</sup>	F <sub>1</sub> <sup>c</sup>	F <sub>2</sub> <sup>c</sup>
Water content(wt.%)	64.41 ± 0.16	10.77 ± 0.10	75.09 ± 0.42	9.19 ± 0.08
Yield of bio-oil (wt.%)	57.3	42.7	60.5	39.5
Ratio of collected water content of oil <sup>a</sup>	88.9	11.1	92.7	7.3
C (wt.%)	17.07	60.95	10.67	66.56
H (wt.%)	10.76	7.26	11.23	7.50
N (wt.%)	<0.3	0.94	<0.3	1.30
O <sup>b</sup> (wt.%)	71.87	30.85	77.80	24.65
pH	2.84	4.10	3.37	4.40
Density (g/cm <sup>3</sup> )	1.0705	1.1550	1.0392	1.1766
High heating value (MJ/kg)	–	22.06	–	23.86
Na content (ppm)	46	38	19	36
K content (ppm)	19	116	13	41
Ca content (ppm)	82	60	57	23
Mg content (ppm)	8	8	8	1

<sup>a</sup> The total water yield during the reaction process is equal to the sum of the product of mass and water content at each condenser. The ratio of the collected water content of oil for each condenser is equal to the collected water yield at each condenser divided by the total water yield.

<sup>b</sup> By difference.

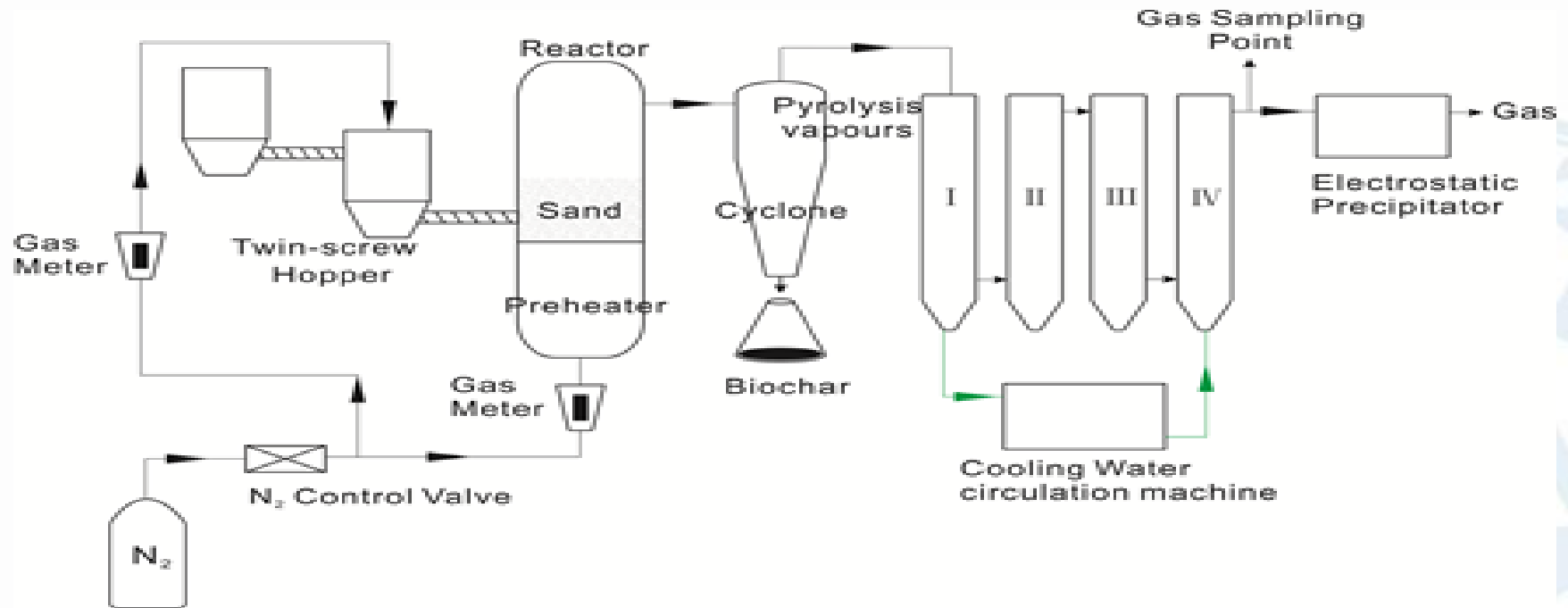
<sup>c</sup> C<sub>1</sub>, C<sub>2</sub> were the bio-oil condensed in the condenser and EP when using the cyclone only to remove the solid particle, and F<sub>1</sub>, F<sub>2</sub> were the bio-oil condensed in the condenser and EP when using the cyclone coupled with HVF.

## Conclusion:

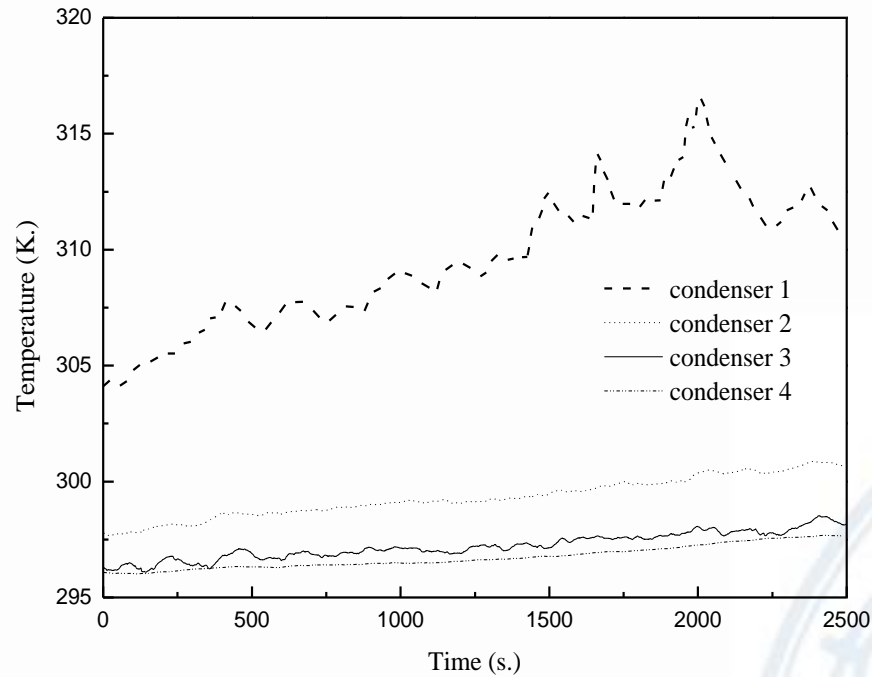
It was found that the total bio-oil yield decreased and that the bio-oil has a higher water content, higher pH value, and lower alkali metal content when a HVF is used in the system.



# \*Effect of Selective Condensation on the Characterization of Bio-oil from Pine Sawdust Fast Pyrolysis Using a Fluidized-Bed Reactor



The flow chart of the fluidized bed reactor fast pyrolysis system



The temperature changes of the four condensers



## (1) Yield and the Water Content of the Bio-oil at Different Condensers

**Yield and the Water Content of the Bio-oil at Different Condensers**

	Condenser 1 <sup>#</sup>	Condenser 2 <sup>#</sup>	Condenser 3 <sup>#</sup>	Condenser 4 <sup>#</sup>	Condenser 5 <sup>#</sup>
Yield of bio-oil (wt/%)	65.3	1.8	1.2	11.3	20.4
Water content(wt/%)	33.21	7.82	7.45	7.35	7.45
Ratio of collected water content of oil <sup>a</sup>	86.2	0.6	0.4	3.3	9.5

Note: <sup>a</sup> The total water yield during the reaction process was equal to the sum of the product of mass and water content at each condenser. The ratio of the collected water content of oil for each condenser is equal to the collected water yield at each condenser divided by the total water yield .

**Conclusion 1** : The total bio-oil, the gases and the char yields were 41.5%, 43.3%, 15.2% respectively ; and 86.2 wt % water steam was condensed in condenser 1.



## (2) Other properties



### pH Value of the Bio-oil

	1 <sup>#</sup>	2 <sup>#</sup>	3 <sup>#</sup>	4 <sup>#</sup>	5 <sup>#</sup>
pH	2.66	2.73	2.78	2.78	2.78

### Higher Heating Value (HHV) of the Bio-oil

	1 <sup>#</sup>	2 <sup>#</sup>	3 <sup>#</sup>	4 <sup>#</sup>	5 <sup>#</sup>
HHV (MJ/Kg)	14.9	22.6	22.9	22.7	23.5

### The Effect of Temperature on the Viscosity of Bio-oil

	20 °C	30 °C	40 °C	50 °C	60 °C	70 °C	80 °C	90 °C
<b>Viscosity</b> of bio-oil 1 <sup>#</sup> (mm <sup>2</sup> /s)	9.10	1.95	1.35	1.21	0.94	0.63	0.54	0.53
<b>Viscosity</b> of bio-oil 4 <sup>#</sup> (mm <sup>2</sup> /s)	938.13	326.09	142.38	69.25	38.01	12.93	7.26	5.80
<b>Viscosity</b> of bio-oil 5 <sup>#</sup> (mm <sup>2</sup> /s)	1210.97	397.44	175.48	82.50	46.87	26.88	17.48	12.62

**Conclusion 2:** The bio-oil condensed in the later condensers has a lower water content, higher pH value, higher heating value, higher kinetic viscosity compared to the first one.



**Table 8. Components of Bio-oil from Pine Sawdust Pyrolysis and Their Relative Mass Contents Detected by GC-MS**

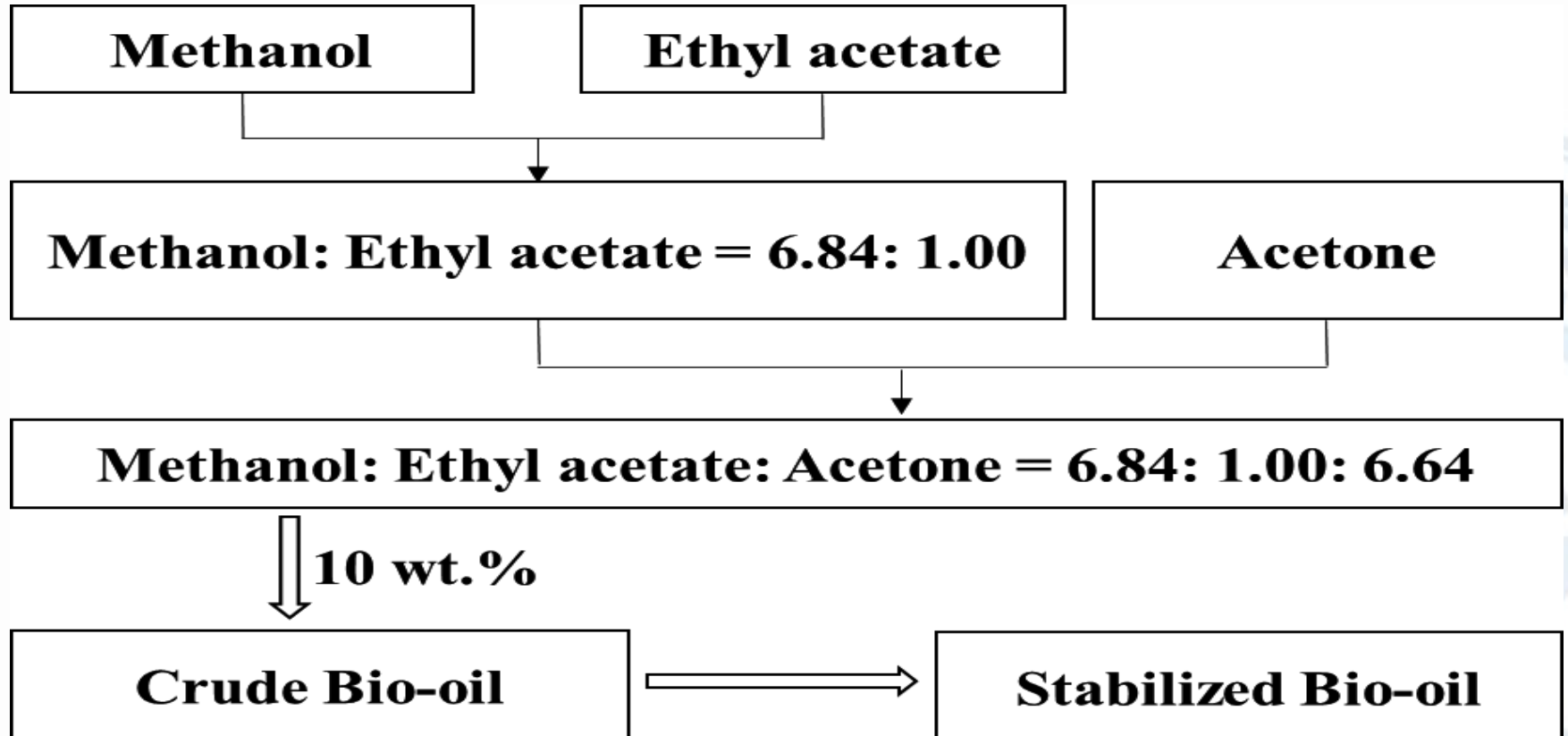
Peak NO.	Main identified compounds	RTA(min)	mol mass	Relative mass content (%)		
				1#	4#	5#
1	Ethynyl isopropyl ketone	3.552	96	0.15		
2	1,3-dione-4-Cyclopentene	3.642	96	1.21	0.21	0.2
3	Cyclopentanone	3.883	84	4.98		
4	2(5H)-Furanone	3.896	84		3.5	2.67
5	2-Methyl-2-cyclopentenone	4.124	96	3.92	1.41	1.24
6	1-(2-furanyl)-Ethanone,	4.227	110	1.18	0.32	0.38
7	3-methyl- 2,4-Pentanedione	4.314	114		0.27	
8	3-methyl- 2,5-Furandione	4.308	112	0.73		0.45
9	2-methyl-Cyclopentanone	4.448	98	9.98	6.68	6.11
10	Bicyclo[3.1.0]hexan-2-one	4.5	96			0.24

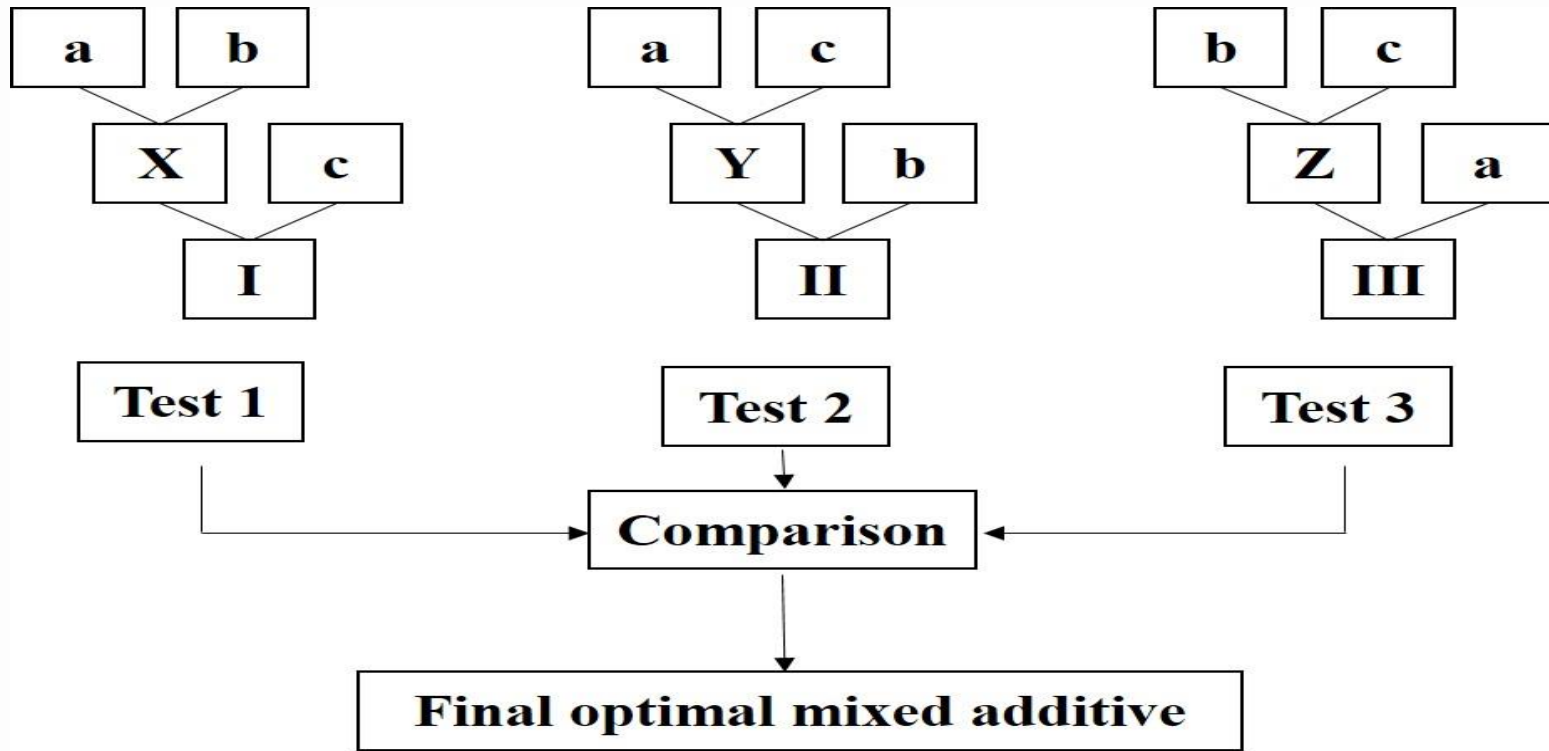
**Conclusion 2:** GC-MS showed that 102 types of chemical compounds were detected and most of the compounds were condensed at different condensers. The selective condensation is useful to separate the water and chemical compounds from bio-oil compared with direct contacting condensing.





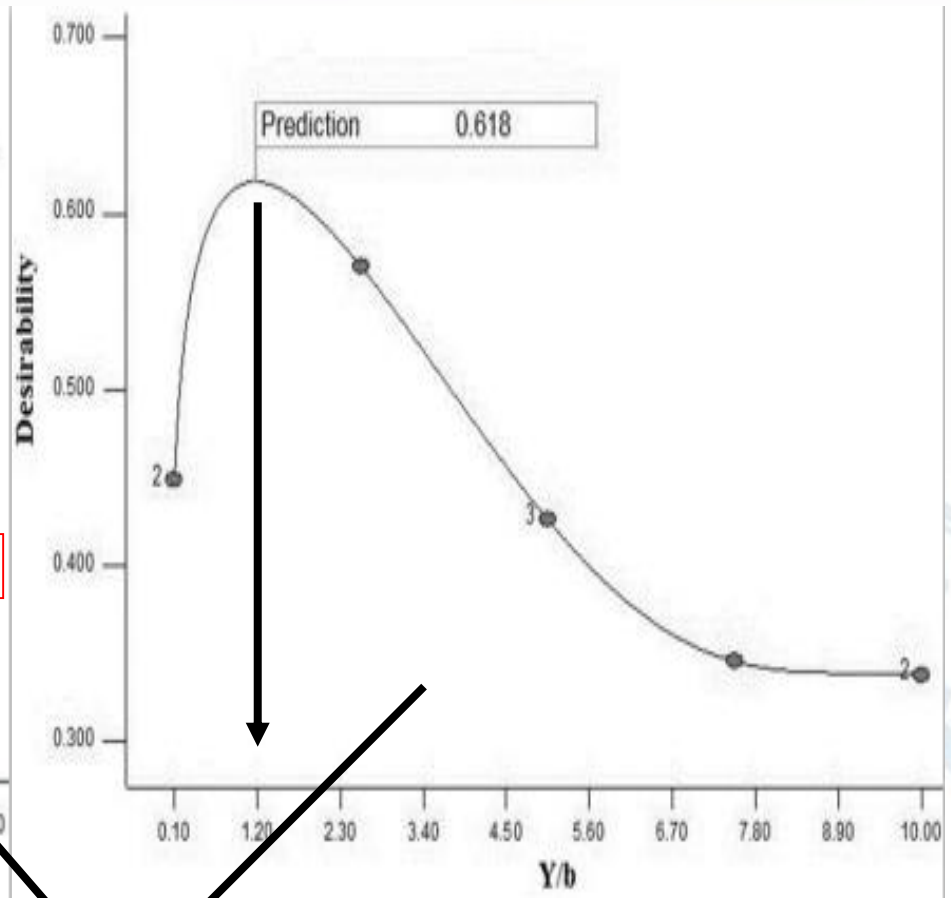
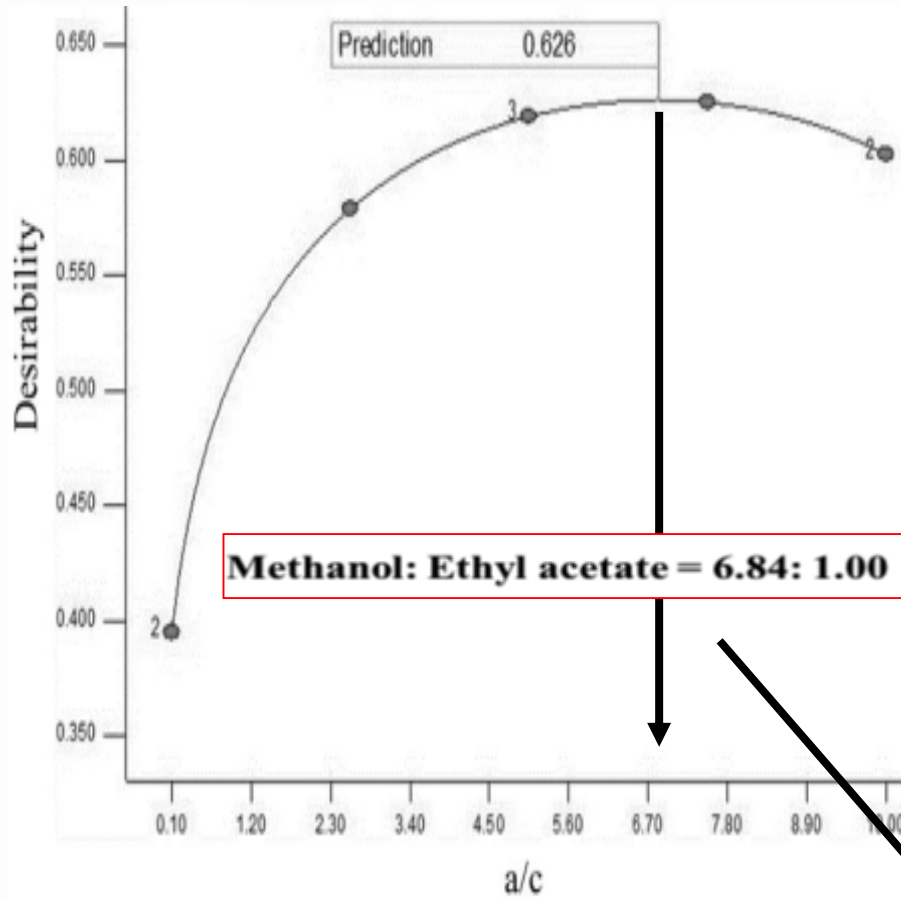
# \*Optimization of a Mixed Additive and its Effect on Physicochemical Properties of Bio-Oil





The diagram of the whole optimization experiment

a      methanol  
b      acetone  
c      ethyl acetate



**Methanol: Ethyl acetate: Acetone = 6.84: 1.00: 6.64**

Optimization curves of the proportion of (1) a to c and (2) Y to b



**Project Title:** Development of Equipment for Biomass  
Fast Pyrolysis for Bio-oil Production and its  
Demonstration in Thousand Ton Scale

**Organizer:** Shanghai JiaoTong University

**Partners:**1) Zhejiang University

2)Shandong University of Technology

3)Guangzhou Institute of Energy Conversion, Chinese  
Academy of Science

4)University of Science and Technology of China

5) University of Science and Technology of South China

6)Liaoyang Hengxing Company Ltd

**Coordinator of the project:** Ronghou Liu

**Period:** January 2011–December 2013

**Budget from MOST:** 11.76 Million RMB Yuan



**A demonstration plant of biomass fast pyrolysis with bio-oil yield:10000 t/a in Shaanxi has been jointly built by Shanxi Yingjiliang Company and Shanghai Jiao Tong University, China**







## 4. Biochar Application for Soil Amendment

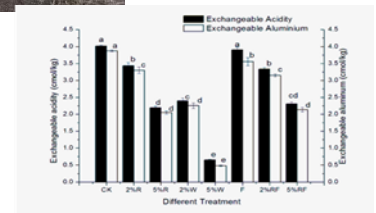
-863 Project by MOST

1) Developed a biochar application machine:  
Scale 4753.8-34185.2 kg/h



2) The effect of biochar on soil and plant growth

wood sawdust biochar could reduce the exchangeable acidity and aluminum by 84% and 88%, respectively at the 5% biochar amendment level.







## 5. Biomass gasification



**Abandoned peach branches**



**Biomass gasification device**

**Utilization of  
the agriculture  
wastes**



**Gas holder**



**Clean combustible gas**



## Impacts of main factors on bioethanol fermentation from stalk juice of sweet sorghum by immobilized *Saccharomyces cerevisiae* (CICC 1308)

Ronghou Liu \*, Fei Shen

Biomass Energy Engineering Research Centre, School of Agriculture and Biology, Shanghai Jiao Tong University, 2678 Qi Xin Road, Shanghai 201101, P.R. China

Received 17 October 2006; received in revised form 17 January 2007; accepted 17 January 2007  
Available online 13 March 2007

### Abstract

In order to attain a higher ethanol yield and faster ethanol fermentation rate, orthogonal experiments of ethanol fermentation with immobilized yeast from stalk juice of sweet sorghum were carried out in the shaking flasks to investigate the effect of main factors, namely, fermentation temperature, agitation rate, particles stuffing rate and pH on ethanol yield and CO<sub>2</sub> weight loss rate. The range analysis and analysis of variance (ANOVA) were applied for the results of orthogonal experiments. Results showed that the optimal condition for bioethanol fermentation should be A<sub>4</sub>B<sub>3</sub>C<sub>3</sub>D<sub>4</sub>, namely, fermentation temperature, agitation rate, particles stuffing rate and pH were 37 °C, 200 rpm, 25% and 5.0, respectively. The verification experiments were carried out in shaking flasks and 5 L bioreactor at the corresponding parameters. The results of verification experiments in the shaking flasks showed that ethanol yield and CO<sub>2</sub> weight loss rate were 0.807% and 1.020 g h<sup>-1</sup>, respectively. The results of ethanol fermentation in the 5 L bioreactor showed that ethanol yield and CO<sub>2</sub> weight loss rate were 0.807% and 1.020 g h<sup>-1</sup>, respectively.

**This paper has been Top 20 Articles, in the Domain of Article 17360181, Since its Publication (2008)**

### 1. Introduction

Ethanol production as an alternative fuel energy resource has been a subject of great interest since the oil crisis of the 1970s (Tao et al., 2005). Therefore, a strong need exists for efficient ethanol production with low cost in raw material and production process. The varied raw materials used in the production of ethanol via fermentation are conveniently classified into three main types of raw materials: sugars, starches, and cellulose materials. Sugars (from sugarcane, sugar beets, sweet sorghum, molasses, and fruits) can be converted into ethanol directly. Starches (from corn, cassava, potatoes, and root crops) must firstly be hydrolyzed to fermentable sugars by the action of enzymes from

malt or molds. Cellulose (from wood, agricultural residues, waste sulfite liquor from pulp, and paper mills) must likewise be converted into sugars, generally by the action of mineral acids. Once simple sugars are formed, enzymes from microorganisms can readily ferment them to ethanol (Lin and Tanaka, 2006). As for materials, one of the prime sources being investigated for ethanol is sweet sorghum. Sweet sorghum (*Sorghum bicolor* (L.) Moench) is a high biomass- and sugar-yielding crops (Bryan, 1990), meantime, the stalk of sweet sorghum contains quite a few quantities of soluble (glucose and sucrose) and insoluble carbohydrates (cellulose and hemicellulose) (Jasberg et al., 1983). Therefore, of many crops currently being investigated for energy and industry, sweet sorghum is one of the most promising, particularly for ethanol production (Gnansounou et al., 2005).

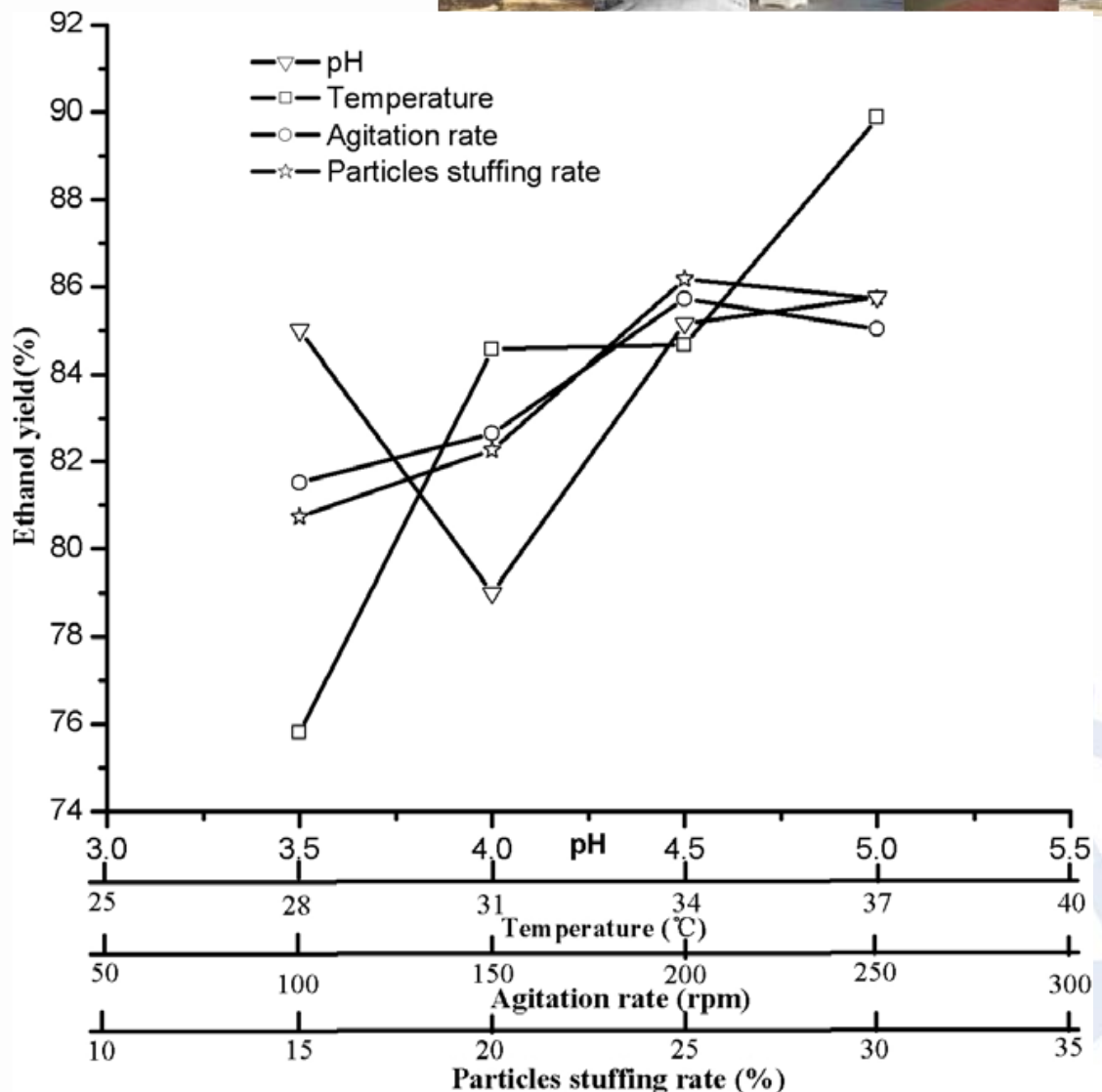
The advantages of immobilized cells over free cell systems have been extensively reported (Pleissner et al., 2007).

\* Corresponding author. Tel.: +86 21 64783844; fax: +86 21 64193285.  
E-mail address: [liuronghou@sjtu.edu.cn](mailto:liuronghou@sjtu.edu.cn) (R. Liu).

## Optimal condition for bioethanol fermentation:

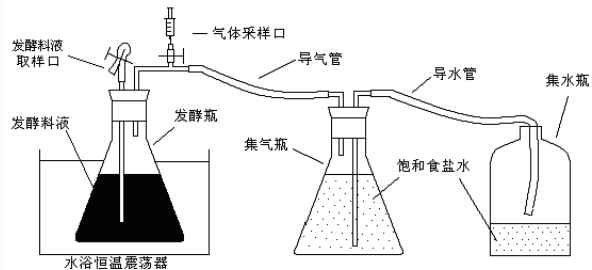
Fermentation temperature:  $37^{\circ}\text{C}$ ,  
agitation rate 200 rpm,  
particles stuffing rate: 25%,  
pH 5.0.  
Ethanol yield: 98.07%,  
Fermentation time 11

h.





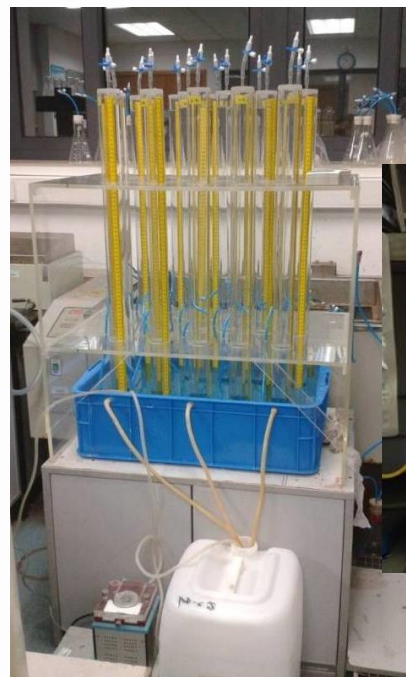
## 7. Biogas



**Fermentation device design**



**BMP Test device and  
CSTR Reactor**



**Experimental apparatus**

# Impacts of Alkaline Hydrogen Peroxide Pretreatment on Chemical Composition and Biochemical Methane Potential of Agricultural Crop Stalks

Chen Sun,<sup>†,‡,§</sup> Ronghou Liu,<sup>\*†,§</sup> Weixing Cao,<sup>§</sup> Renzhan Yin,<sup>||</sup> Yuanfei Mei,<sup>†,‡,§</sup> and Le Zhang<sup>†,§</sup>

## Objective:

to increase bio-digestibility and methane yield from crop residues via pretreatment

## Results and conclusions:

### The AHP pretreatment could:

- break down esterified and etherified linkage in lignocellulose
- recover 90% of glucose and 80% of xylose;
- remove 30-50% of lignin;
- increased methane yield and bio-digestibility for certain biomass

It is necessary to utilize of the liquid waste from the pretreatment.

Impacts of Alkaline Hydrogen Peroxide Pretreatment on Chemical Composition and Biochemical Methane Potential of Agricultural Crop Stalks

Chen Sun,<sup>†,‡,§</sup> Ronghou Liu,<sup>\*†,§</sup> Weixing Cao,<sup>§</sup> Renzhan Yin,<sup>||</sup> Yuanfei Mei,<sup>†,‡,§</sup> and Le Zhang<sup>†,§</sup>

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**ABSTRACT:** Lignocellulosic stalks of three kinds of monocotyledonous (wheat, maize, and rice) and two kinds of dicotyledonous crops (rape and cotton) underwent 28 h H<sub>2</sub>O<sub>2</sub> pretreatment at pH 11.5 and 10 °C with 10% (w/v) biomass loading. Chemical composition analysis and biochemical methane potential (BMP) assays were carried out for biomass before and after pretreatment, in order to evaluate the impact on biomass methane efficiency caused by the alkaline hydrogen peroxide (AHP) pretreatment. The AHP pretreatment could remove about 30% of glucose and 80% of xylose, and recover about 10% and 91–100% of the lignin in monocotyledonous and dicotyledonous crop stalks, respectively. On the basis of starch and cellulose (V<sub>5</sub>) added into the pretreatment system, the observed BMP and digestible fraction of cotton stalk increased from 13.9 g CH<sub>4</sub>/g V<sub>5</sub> and 31.6 g CH<sub>4</sub>/g V<sub>5</sub> to 21.6 g CH<sub>4</sub>/g V<sub>5</sub> and 36.0 g CH<sub>4</sub>/g V<sub>5</sub>, respectively. For the purpose of full utilization, the chemical composition and BMP of liquid waste generated from the AHP pretreatment were investigated. Theoretically, around 15 mol CH<sub>4</sub>/g CH<sub>2</sub>O from liquid waste of monocotyledonous and dicotyledonous crop stalks could be produced, respectively. Finally, chemical composition and structural change showed that AHP pretreatment could break down esterified and etherified linkage in a lignocellulosic matrix.

### 1. INTRODUCTION

Lignocellulosic materials such as agricultural crop straws and stalks are renewable resources in the world. They mainly consist of cellulose, hemicellulose, and lignin, and are considered as potential sources of energy.<sup>1</sup> However, the lignocellulosic materials are difficult to be degraded by anaerobic bacteria because of their complex organic polymer structures.<sup>2</sup> The close physical and chemical association among the cellulose, hemicellulose, and lignin in lignocellulosic materials is a major limitation to their efficient utilization.<sup>3</sup> The major degradation pretreatment of lignocellulosic material is to cut the long glycosidic bonds in the area of initial production or secondary utilization.<sup>4</sup>

There are numerous pretreatment methods for lignocellulosic materials, and they can be classified as physical (cutting, thermal, etc.), chemical (acid dilution, oxidation, etc.), and biological methods.<sup>5</sup> One of the most promising chemical methods for degradation is alkaline hydrogen peroxide (AHP) pretreatment.<sup>6</sup> It was reported that the phenolic units of lignin had a high tendency to destroy in AHP solution.<sup>7</sup>

During AHP pretreatment, the peroxide plays the role of oxidant,<sup>8</sup> which takes part in the various degradation process and has been widely used to bleach high-purity wood pulp in the paper-making industry. The role of alkaline is to reduce or to remove lignin, tannin, and other extractives.

As a pretreating method, lots of studies have been done on the AHP pretreatment process conditions in order to improve its efficiency on degradation, sugar recovery, and biogas production. Mass and Lalonde (2011) found that treatment at 1% when using 3% H<sub>2</sub>O<sub>2</sub> solution at 60 °C with pH 11.5 could reach 77% reduction, 63% xylan, and 80% xanthanase release.<sup>9</sup> Terasmaa et al. (2000) used 1% (v/v) H<sub>2</sub>O<sub>2</sub> and 1 wt % NaOH solution which was actually a mild AHP.

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ACS Publications

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DOI: 10.1021/acs.energyfuels.5b01896

Energy Fuels 2015, 29, 1896–1904



## Selected Publications(SCI)

- 1) Tianju Chen, Ceng Wu, Ronghou Liu, et al. Effect of hot vapor filtration on the characterization of bio-oil from rice husks with fast pyrolysis in a fluidized bed reactor[J]. **Bioresource Technology**, 2011, 102, 6178-6185.
- 2) Tianju Chen, Chunjian Deng, and Ronghou Liu. Effect of Selective Condensation on the Characterization of Bio-oil from Pine Sawdust Fast Pyrolysis Using a Fluidized-Bed Reactor [J]. **Energy & Fuels**, 2010, 24 (12), pp 6616–6623.
- 3) Tianju Chen, Ceng Wu, Ronghou Liu. Steam reforming of bio-oil from rice husks fast pyrolysis for hydrogen production[J]. **Bioresource Technology**, 2011, 102, 9236-9240.
- 4) Ronghou Liu, Fei Shen. Impacts of main factors on bioethanol fermentation from stalk juice of sweet sorghum by immobilized *Saccharomyces cerevisiae* (CiCC 1308)[J]. **Bioresource Technology**, 2008, 99, 847-854.
- 5) Le Zhang, Ronghou Liu, Renzhan Yin, Yuanfei Mei. Upgrading of bio-oil from biomass fast pyrolysis in China: A review[J]. **Renewable and Sustainable Energy Reviews** 24 (2013) 66–72.





- 6 ) Renzhan Yin, Ronghou Liu, Yuanfei Mei, Wenting Fei, Xingquan Sun. Characterization of bio-oil and bio-char obtained from sweet sorghum bagasse fast pyrolysis with fractional condensers[J]. **Fuel** , Volume 112, October 2013, Pages 96–104.
- 7 ) Ceng Wu, Ronghou Liu. Sustainable hydrogen production from steam reforming of bio-oil model compound based on carbon deposition/elimination[J]. **International Journal of Hydrogen Energy**, 2011, 36, 2860-2868.
- 8 ) Ceng Wu, Ronghou Liu. Carbon deposition behavior in steam reforming of bio-oil model compound for hydrogen production[J]. **International Journal of Hydrogen Energy**, 2010, 35, 7386-7399.
- 9 ) Weixing Cao, Chen Sun, Ronghou Liu, Renzhan Yin, Xiaowu Wu. Comparison of the effects of five pretreatment methods on enhancing the enzymatic digestibility and ethanol production from sweet sorghum bagasse[J]. Bioresource Technology, Volume 111, May 2012, Pages 215–221.
- 10 ) Renzhan Yin, Ronghou Liu, Jinkai Wu, Xiaowu Wu, Chen Sun, Ceng Wu. Influence of particle size on performance of a pilot-scale fixed-bed gasification system[J]. *Bioresource Technology*, 119 (2012) 15–21.



## 8.Conclusion

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Different conversion technologies can treat different types of raw materials, and different product can be obtained, there are both advantages and disadvantages for any conversion technology. Therefore, adequate conversion technology should be chosen according to concrete conditions in order to promote commercialization of biomass energy.



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**Thank you!**

